

## Definition of Rational Conditions of Materials Grinding in Energy-Saving Milling Complex\*

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**Abstract:** Current issues of energy saving in cement production, using technological milling complex, which includes a press roller crusher and ball mill, discussed in the article. Optimized milling conditions of previously ground material through the installation of energy-exchange blade devices (EBD) in a mill drum have been proposed. It was found that the level of charge by grinding media in the first chamber periodically varies according to the rotation angle of the mill drum equipped with EBD. There is a "scooping" of the grinding media with a grinding material in the zone of active influence of EBD along, lifting them to a height and enforcing them a cross-longitudinal movement. All that is different from being created in the ball mills without EBD. The additional work is performed, which consumes engine power. Method of calculating an additional power consumption of the mill drive equipped with EBD was proposed; additional power expended to create cross-longitudinal motion of the grinding media in the first and second chambers in its areas of active influence of EBD. The comparative analysis of the results obtained by experiment and calculation on the proposed equations showed high convergence results. The analytical dependencies may be of interest for both Russian and foreign organizations operating in the design and manufacture of cement equipment, as well as for cement manufacturers.

**Key words:** Energy intensity • Complex of grinding • Press roller grinder • Ball mill • Method of calculation • Additional power consumption • Energy-exchange blade devices

### INTRODUCTION

Among the most energy-intensive processes are the processes of crushing and mill grinding materials, which consumes about 10% of the world's electricity in the production of binders, different mixes and products. At the same time, power consumption increases significantly within increasing a product fineness.

It is known, that power consumption for crushing is 10-21 J/g and 360-3600 J/g for fine and super fine grinding [1].

Therefore, studies aimed at improving the grinding technology and equipment to reduce energy intensity of the process are relevant.

In cement production with the annual volume, which is continuously increasing in the world and currently more than 2.5 billion tons, the processes of

mill grinding materials and cement, undertaken mainly in ball mills, expend from 40 to 70% of all electricity in the process [2].

Scholars and practitioners in our country and abroad are involved in developing new machines and improving the efficiency of existing milling equipment [4-8].

Energy-saving technology for the grinding of cement was developed by them as a complex consisting of two units of a press roller grinder and a ball mill (PRG-BM) [9-11].

### RESULT AND DISCUSSION

The studies found that the milled material in PRG after the pressure treatment between the rolls is significantly different from the original. Material presents in the form of pressed plates and its



Fig. 1: Feed material(clinker)



Fig. 2: Clinkergroundin the PRG

particles have microdefect structure that requires special conditions for their milling in the ball mills (Fig. 1, 2).

The material, that was pre-ground in PRG, is subject to momentary force impact in the first mill chamber for disagglomeration compacted material by abrasion-grinding effect of the grinding media in the second mill chamber for its final milling, study revealed. Such conditions can be obtained by grinding the materials in a ball mill, equipped with energy-exchange blade devices (EBD), double acting blade (DAB) and elliptical blade segment (EBS).

To determine the operating modes of grinding media for different schemes of EBD setup, studies were carried out on the model of a ball mill with a transparent body of  $\varnothing 0,1 \times 0,5$  m size (Fig. 3a-d), at a small innovative company "Center of energy-saving technologies and systems" based on innovative business incubator Belgorod State Technological University named after V.G. Shoukhov within the states support innovative entrepreneurship of young scientists in Russian universities [12].

The studies found, that the nature of the dynamic impact of the grinding bodies in the BM is under substantial influence of the relative position EBD, both longitudinally and in cross section of the mill drum.

Thus, when EBD is set at the discharge end of the mill drum and inclined to the bottom of it, or its major axis coincides with the major axis DAB (Fig. 3a) the

simultaneous effect of grinding media appears, with a  $360^\circ$  spacing. This leads to concentration of the grinding bodies in the middle of the second chamber, which negatively affects the efficiency of a grinding process.

Turning the EBD relatively to the DAB at  $180^\circ$  (displacement of the major axes at the  $180^\circ$  angle) leads to alternate impact of the EBD on the grinding media, leading to their greater mobility, displacement and concentration, here at the DAB and then at the EBD (Fig. 3b). Such EBD setup schemes should facilitate intensity of the process of grinding the pre-ground material in the second chamber of the mill.

However, setting the EBD, tilted to the bottom of the discharge end, results in the capture of the grinding media by EBD and lifting it to greater heights, which leads to a partial water fall work mode, which will reduce its effectiveness in the second chamber.

Changing the tilt angle of EBD to the opposite, setting it at an angle from the discharge end (Fig. 3), results in the "waterfall effect" vanishing in the second mill chamber. Since, such a location of EBD does not lift the grinding media, but only increases its impact in the longitudinal direction; it positively affects the grinding material.

Turning the EBD relatively to the DAB at the angle other than  $180^\circ$  (e.g.  $90^\circ$  or  $270^\circ$ ) leads to partial concentration of the grinding media in the chamber center (Fig. 3g). It comes from the overlap of the pulses from the impact of DAB and EBD, which also negatively affects the efficiency of the grinding process.

Installation of double action blades will provide as hock-abrading effect of the grinding media to the grinding material in the first mill chamber. Controlling the pulse range of DAB, besides the angle of inclination, ensures the presence of horizontal sections of the diaphragm.

Thus, the research of the nature of the grinding media motion in the BM equipped with EBD showed that the work mode of the grinding media depends on the setup scheme and arrangement of DAB and EBD. Rational EBD setup scheme in a mill drum for grinding pre-ground materials in PRG is a diagram (Fig. 3c), where the shock-abrasive effect of the grinding media in the first mill chamber and the crushing-abrading effect in the second.

Installation of energy-exchange blade devices in the form of a double-acting blade (DAB) and blade elliptical segment (EBS) in the ball mill drum allows intensifying the grinding media studies have shown. However, the level of the grinding media in the first chamber varies periodically according to the rotation angle of the mill drum; and in the active zone of EBD influence "scooping" of the grinding

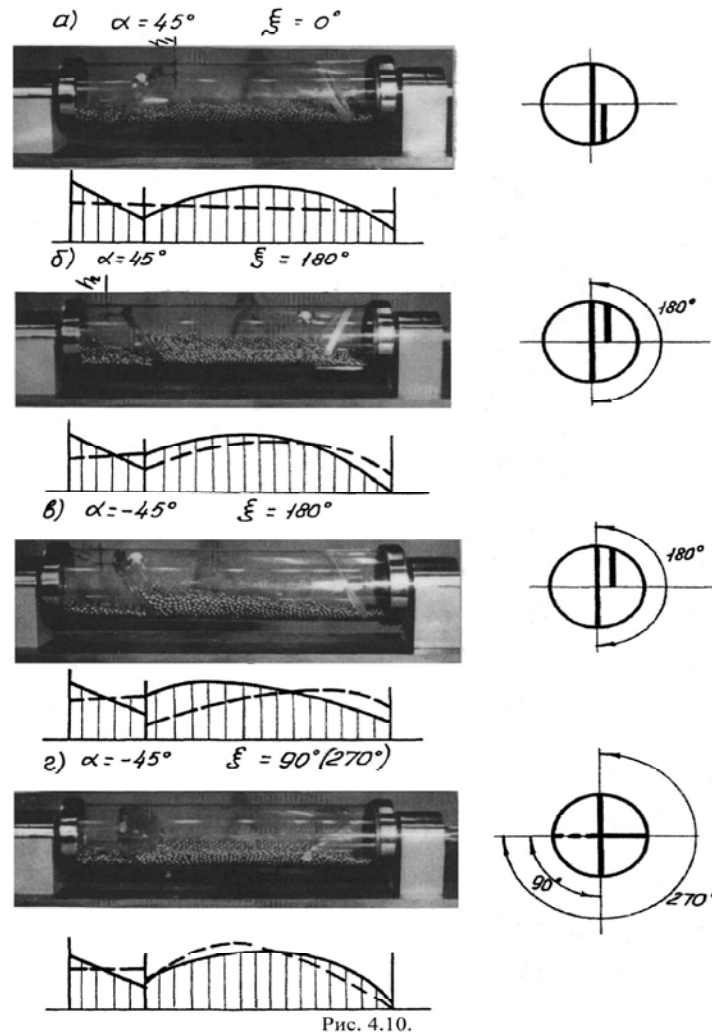


Рис. 4.10.

Fig. 3: Setup diagrams EBD in BM and diagrams of the movement of grinding media

media with grinding material occurs, lifting them to a height and giving them cross-longitudinal movement, unlike produced in mills without EBD (Fig. 4). At the same time, take additional work, which increases the power consumption. Lack of scientific methodology for calculating the amount of power for mills equipped with EBD in hibiits their adoption by the industry.

Additional power consumption of the mill connected (compared with wind mills with vertical partitions) with reposition of the center of the grinding media mass along the axis of the mill drum, by influencing the grinding media in the long itudinal direction of DAB and EBD.

Power  $N$  for a certain period of time  $T$  is calculated by the for mula:

$$N = \frac{A}{T}, \quad (1)$$

where,  $A$  -the work donefor the sameamount of time  $T$ .

The time taken for onerevolution of the milldrum, over theperiod of time  $T$ , when the millperformsnrevolutions per minute, allowsone revolutionto occurin a timeequal to:

$$T = \frac{1}{n}; \text{ min} \quad (2)$$

or

$$T = \frac{60}{n}; \text{ sec} \quad (3)$$

because

$$n = \psi n_{\text{eo}} \quad (4)$$

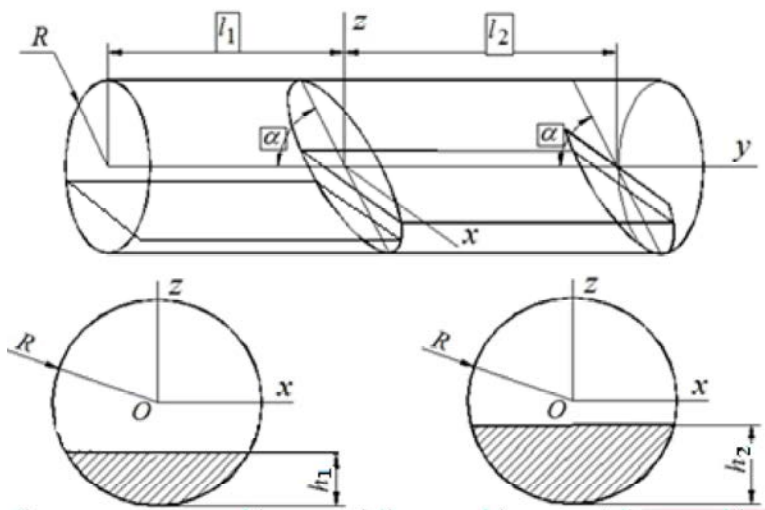


Fig. 4: Setup scheme of EBD in the ball mill drum

where,  $\Psi$  [Psi] – relative rotation speed;  $n_{kp}$  – a critical rotation speed.

Since,

$$n_{kp} = \frac{30}{\pi} \sqrt{\frac{g}{R}} \quad (5)$$

where,  $g = 9,81 m/s^2$  – acceleration of gravity;  $R$  – the radius of the mill drum; formula (3) can be written as:

$$T = \frac{2\pi\sqrt{R}}{\Psi\sqrt{g}}; \text{ sec} \quad (6)$$

During one revolution of the mill drum, the center of the grinding media mass in each chamber will move from one extreme position to the other and back again.

For the first chamber relocation of the center of the grinding media mass per revolution of the mill drum is determined by the formula:

$$S_1 = 2|y_c - y'_c| \quad (7)$$

According to [6],  $y_c$  and  $y'_c$  are calculated by the formulas, respectively:

$$\begin{aligned} \tilde{y}_c \tilde{V}_1 = & -\frac{\lambda_1^2}{2} \left( \chi_1 \sqrt{1 - \chi_1^2} + \arcsin \chi_1 - \frac{\pi}{2} \right) - \frac{2\lambda_1 \text{ctg} \alpha}{3} (1 - \chi_1^2)^{\frac{3}{2}} + \\ & + \frac{\text{ctg}^2 \alpha}{8} \left( \chi_1 (1 - 2\chi_1^2) \sqrt{1 - \chi_1^2} - \arcsin \chi_1 + \frac{\pi}{2} \right). \end{aligned}$$

$$\begin{aligned} \tilde{y}'_c \tilde{V}'_1 = & -\frac{\lambda_1^2}{2} \left( \chi'_1 \sqrt{1 - \chi'^2_1} + \arcsin \chi'_1 - \frac{\pi}{2} \right) + \frac{2\lambda_1 \text{ctg} \alpha}{3} (1 - \chi'^2_1)^{\frac{3}{2}} + \\ & + \frac{\text{ctg}^2 \alpha}{8} \left( \chi'_1 (1 - 2\chi'^2_1) \sqrt{1 - \chi'^2_1} - \arcsin \chi'_1 + \frac{\pi}{2} \right). \end{aligned}$$

The center of the grinding media mass relocation per one drum revolution in the second mill chamber is determined by the formula:

$$S_2 = 2|y_{c2} - y'_{c2}| \quad (8)$$

The calculation of  $y_{c2}$  and  $y'_{c2}$ , according to (4) by the formula:

$$\begin{aligned} \tilde{y}_{c2} \tilde{V}_2' &= \frac{\text{ctg}^2 \alpha}{8} \left( \chi_2 (2\chi_2^2 - 1) \sqrt{1 - \chi_2^2} + \arcsin \chi_2 - \frac{\pi}{2} \right) - \\ &- \frac{\lambda_2^2}{2} \left( \chi_2 \sqrt{1 - \chi_2^2} + \arcsin \chi_2 - \frac{\pi}{2} \right). \\ \tilde{y}_{c2} \tilde{V}_2'' &= \frac{\lambda_2^2}{2} \left( \frac{\pi}{2} - \arcsin \chi_2' - \chi_2' \sqrt{1 - \chi_2'^2} \right) + \frac{2l_2 \text{ctg} \alpha}{3} \sqrt{(1 - \chi_2'^2)^3}. \end{aligned}$$

Because the force of friction does the work, then:

$$A = |F_{\text{тп}} S| = F_{\text{тп1}} S_1 + F_{\text{тп2}} S_2 \quad (9)$$

In turn,

$$F_{\text{од1}} = f G_1 = f M_1 g = f g \gamma V_{1\text{своб}} = f g \gamma \varphi_1 V_1 \quad (10)$$

where,  $f$  – coefficient of sliding friction of the grinding media with the mill drum body;  $G_1$  – load weight of the grinding media in the first chamber;  $M_1$  – mass of the grinding media in the first chamber;  $\gamma$  [gamma] – volume weight of the grinding media;  $V_{1\text{своб}}$  – volume of the grinding media in the first chamber;  $\varphi_1$  [fi] – coefficient of charge of the first chamber by the grinding bodies;  $V_1$  – volume of the first chamber.

A similar formula holds for a second camera:

$$F_{\text{тп2}} = f G_2 = f M_2 g = f g \gamma V_{2\text{своб}} = f g \gamma \varphi_2 V_2 \quad (11)$$

Comparative results, obtained by calculation and experiment for the following values of input parameters, are following: radius of the mill drum,  $R=0.5$  m; length of the first chamber,  $l_1=0.65$  m; degree of charge of the first chamber,  $\square_1=0.18$ ; length of the second chamber,  $l_2=1.3$  m; degree of charge of the second chamber,  $\square_2=0.3$ ; coefficient of sliding friction,  $f=0.4$ ; volume weight of the grinding media  $\gamma=4550$  kg/m<sup>3</sup>; angle of DAB and EBD to the axis of the drum mill,  $\alpha=60^\circ$ ; relative rotation frequency of the drum mill (corresponding)  $\Psi=0.76$ .

The divergence between experimentally determined and calculated values do not exceed 10%, results showed. At the indicated values of the input parameters, the additional power consumption, obtained by calculation was 62.2 W for the first camera, 441.0 W for the second camera for and 503.2 W in general for the mill; the experimentally obtained was 545.0 W.

The analysis of the plots of (Fig.5-8), allowed study of the influence of the first chamber length (length of the second chamber, was such that the sum of chambers length equaled to the length of the mill- 1.95 m), tilt angle of EBD and degree of charge factors of the first and second chambers, on the additional power consumption.

The following designation are indicated in the graphs:  $N_1$  and  $N_2$  – additional power consumption by relocation the grinding media in the first and second chambers, respectively;  $N^1$  – designed to additional power consumption; and  $N^3$  - total power consumption measured experimentally.

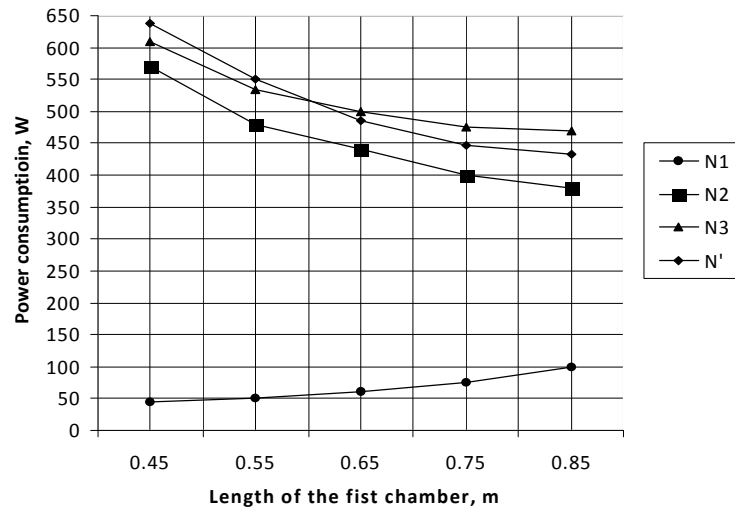


Fig. 5: Dependence between power consumption and length of the first chamber

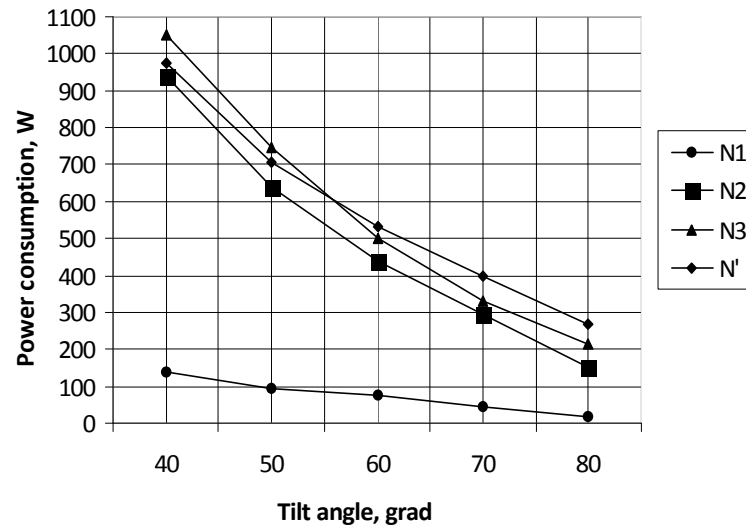


Fig. 6: Dependence between additional power consumption and angle of DAB and EBD to the axis of the mill drum

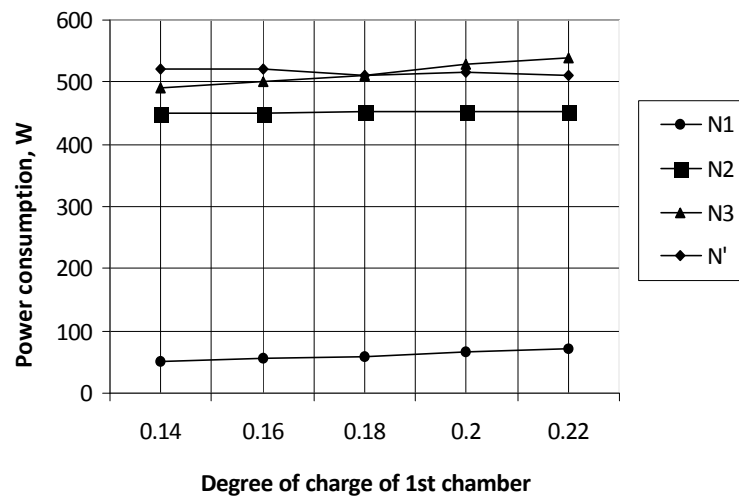


Fig. 7: Dependence between additional power consumption and degree of charge of the first chamber

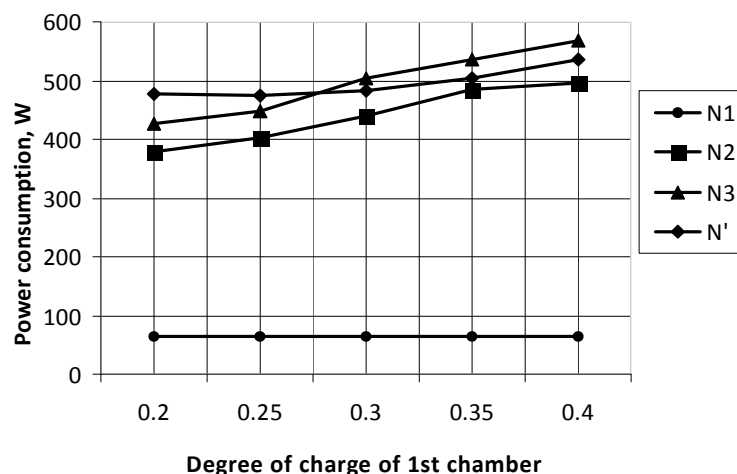


Fig. 8: Dependence between additional power consumption and degree of charge of the second chamber

Installation of energy-exchange device in the mill drum allows intensifying the work of grinding media, as indicated by the value of an additional power consumption of the mill drive, as can be seen from the plots (Fig. 5-8). Changing the length of the first chamber, in the direction of increasing it, results in a reduction of the total charge of the grinding bodies in the mill drum, which simultaneously leads to a reduction of power consumption by the mill drive and grinding quality deterioration (Fig. 5). Optional length of the first chamber for pre-grinding of a clinker of deformed structure is 0.65m, which is 1/3 of the total length of the ball drum mill.

The graphic dependence analysis (Fig. 6) showed, that changing the tilting angle of energy-exchanging blade devices to the axis of the mill drum, from 40° to 80°, leads to a further reduction in power consumption. It happens because the zone of influence of DAB decreases and in the second chamber, the zone of influence of BES on the grinding media, which leads to further reduction in power consumption. Increasing the degree of charge by the milling bodies in the first mill chamber from 0.14 to 0.22 and the second from 2.2 to 0.4 (Fig. 7 and 8), leads to an increase in the total weight of the grinding bodies in the mill drum, that proportionally affects the growth of the additional power consumption of the machine.

## CONCLUSION

The comparative analysis of plots (Figure 5-8), based on the data obtained experimentally and by calculations, shows that the divergence between the experimentally determined and calculated values do not exceed 10%.

Thus, the installation of the energy-exchange devices in the mill drum allows intensifying the work of grinding media. This is indicated by the value of the additional power consumption of the mill drive.

Analytically obtained equations (10) and (11) allow us to calculate the additional power consumption of the mill, equipped with EBD and with sufficient accuracy, to show the real grinding process.

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